



## RESEARCH ARTICLE

# Revealing the Roles of CuF<sub>2</sub>/NiF<sub>2</sub> Incorporation in the Electrochemical Performance of FeF<sub>3</sub> Cathodes in Solid-State Batteries

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## ABSTRACT

Mixed metal fluorides have been considered as a promising candidate to lower the voltage hysteresis of conversion-type iron fluoride cathodes, but their cycling stability is limited due to transition metal dissolution and interphase growth in liquid electrolyte batteries. Here, we study the role of incorporating CuF<sub>2</sub> and NiF<sub>2</sub> in the electrochemical performance of FeF<sub>3</sub> cathode in halide-based solid-state batteries to test whether we can transfer the kinetic benefit of low voltage hysteresis to solid-state batteries while using solid electrolyte to eliminate transition metal dissolution and stabilize the interphase. Synchrotron X-ray absorption spectroscopy results indicated the redox reactions are attributed to Cu<sup>0</sup>/Cu<sup>+</sup> and Fe<sup>0</sup>/Fe<sup>2+</sup> in 25CuF<sub>2</sub>-75FeF<sub>3</sub> and Ni<sup>0</sup>/Ni<sup>2+</sup> and Fe<sup>0</sup>/Fe<sup>3+</sup> in 10NiF<sub>2</sub>-90FeF<sub>3</sub>. While no apparent improvement in electrode kinetics can be observed, the incorporation of CuF<sub>2</sub> and NiF<sub>2</sub> can largely improve the cycling stability of FeF<sub>3</sub> cathodes. The results demonstrate the advantages of using solid-state concept to improve the cycling stability of conversion-type cathodes.

## 1 | Introduction

The growing interest in electrifying transportation has led to a higher demand for the energy density of lithium-ion batteries (LIBs) [1]. As the energy density of conventional LIBs approach their physicochemical limits [2], conversion-type iron fluorides (FeF<sub>2</sub>/FeF<sub>3</sub>) have received renewed interest as next-generation cathodes because they can accommodate multiple electron transfers per redox center, offering 200% to 300% higher theoretical energy density than state-of-the-art intercalation cathodes, without using expensive and scarce minerals such as Co and Ni [3–12]. Despite these great promises, practical application of these cathodes has proven challenging due to large voltage hysteresis

and limited cycling stability during charge/discharge cycles [11, 13–17]. Since the initial reports in early 2000s, considerable efforts have been made to understand the fundamentals of the reaction mechanisms for the development engineering approaches to address these performance challenges [13, 18–32].

The widely accepted theory of the conversion reaction mechanism is based on reconstructive phase transitions [4, 7, 8]. For FeF<sub>2</sub>, a direct conversion from FeF<sub>2</sub> to LiF and Fe occurs upon lithiation [33]. In the case of FeF<sub>3</sub>, the reaction progresses by an initial reduction via the insertion of Li ions to form Li<sub>x</sub>Fe<sub>y</sub>F<sub>z</sub> intermediate phases and FeF<sub>2</sub>, followed by direct conversion to LiF and Fe [8]. The reductions of both FeF<sub>2</sub> and FeF<sub>3</sub> involve

Keng Xu and Kangxuan Xia equally contributed to this paper.

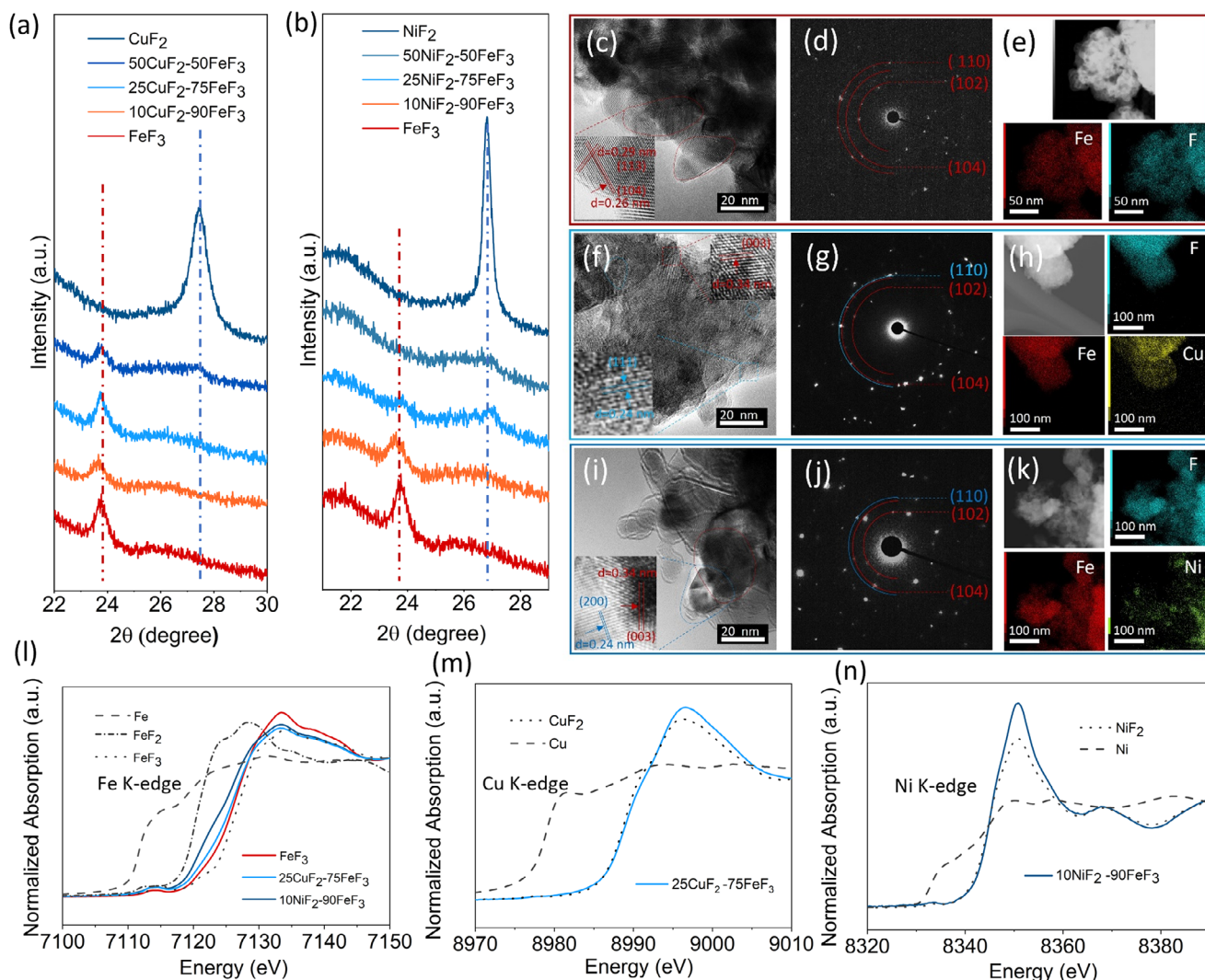
significant changes both chemically and structurally. However, these understandings were challenged by recent studies on characterizing structural evolutions of  $\text{FeF}_2$  and  $\text{FeF}_3$  electrodes during charge/discharge. By in situ visualization of the spatial and crystallographic correlation between the parent and converted phases through TEM, Karki et al., first reported that the reaction mechanism from  $\text{FeF}_2$  to  $\text{LiF}$  and  $\text{Fe}$  is topotactic transformation in nature, involving transport of  $\text{Li}^+$  and  $\text{Fe}^{2+}$  within the F-anion sublattice that retained throughout the entire discharge process [22]. Subsequently, Xiao et al., demonstrated that the reduction of  $\text{FeF}_2$  during discharge involves the formation of intermediate rutile and rocksalt  $\text{Li-Fe-F}$  phases before fully reducing to  $\text{LiF}$  and  $\text{Fe}$ , but reaffirms that the transformation of  $\text{FeF}_2$  to rutile to rocksalt to  $\text{LiF}$  is entirely topotactic involving the intercalation and diffusion of cations in the fluorine anion sublattice [24]. A recent report from Hua et al. also provided additional evidence on the clear topological relationship of the fluorine anion sublattice between the parent and intermediate metal fluorides and  $\text{LiF}$  during the reduction of  $\text{FeF}_3$  [25]. The fundamental knowledge of the reaction mechanisms of both  $\text{FeF}_2$  and  $\text{FeF}_3$  significantly deviates the conventional belief of a “conversion” reaction and highlights the important roles of intermediate phase formation, interfaces, and transition metal mobility for further development of these battery electrodes [26].

On the other hand, various engineering approaches including utilization of various nanocomposites, nanostructuring, cation and anion substitutions, electrolyte formulation, have been developed to address the performance challenges of iron fluoride cathodes [12, 15, 34–45]. Among all the approaches, incorporating another cation through doping, substitutions, or forming a composite, have received intense interest. Introducing small contents of dopants such as  $\text{Ti}$  [46],  $\text{Co}$  [20, 47],  $\text{Cr}$  [48, 49],  $\text{Mn}$  [50],  $\text{Al}$  [51],  $\text{Nb}$  [52], and  $\text{Ni}$  [53] can reportedly change the electronic structure of iron fluorides and thus improve the electronic conductivity. Despite improved rate performances, the effect of these dopants on reducing the voltage hysteresis of iron fluoride cathodes is limited. In 2015, Wang et al. demonstrated that the incorporation of 50 mol%  $\text{CuF}_2$  in  $\text{FeF}_2$  to form a solid solution  $\text{Cu}_{0.5}\text{Fe}_{0.5}\text{F}_2$  can significantly lower the voltage hysteresis of  $\text{FeF}_2$  from 1.6 to 0.5 V [19]. The authors attributed the enhanced kinetics to: (i) during discharge, the formation of  $\text{Cu}$  and  $\text{LiF}$  at high potential from  $\text{Cu}$  conversion helps accelerate  $\text{Fe}$  conversion because of the enhanced electronic conductivity (due to the presence of metallic  $\text{Cu}$ ) and the increased ionic transport at the  $\text{LiF/FeF}_2$  interface and (ii) during charge, the existing  $\text{Fe-F}$  framework and the high mobility of  $\text{Cu}$  ions can lower the nucleation barrier for  $\text{Cu-F}$  formation [19]. This work represents a pioneering example of improving electrode kinetics by cation substitution. The effective enhancement in reaction kinetics is also supported by a recent study from Li et al., that shows the catalytic effect of  $\text{Cu-Fe}$  dual metal nanodomains for reconversion of  $\text{LiF}$  to transition metal fluoride [54]. Despite the enhanced kinetics, a quick capacity decay can be observed for the first few cycles, due to  $\text{Cu}$  dissolution in the liquid electrolytes [19, 55], highlighting the challenges for practical application of these cathodes. Nevertheless, recent work from Gordon et al., [21]. and Huang et al., [23]. suggests that enhanced kinetics may not be achieved for all ternary iron difluorides, as no decreases in the voltage hysteresis can be observed for  $\text{Ni}_x\text{Fe}_{1-x}\text{F}_2$ ,  $\text{Co}_x\text{Fe}_{1-x}\text{F}_2$ , and  $\text{Mn}_x\text{Fe}_{1-x}\text{F}_2$  solid solutions due to enhanced interphase growth from the side

reactions between the ternary fluorides and liquid electrolytes [21, 23]. In addition, although it is more widely reported for  $\text{Cu}$  [55, 56], other transition metals such as  $\text{Ni}$ ,  $\text{Co}$ ,  $\text{Mn}$ , and  $\text{Fe}$  also have slight solubility in common liquid electrolytes [12, 57], leading to active material loss, diffusion of dissolved transition metal to the anodes and thickening of solid electrolyte interphase. Given the large effects of dissolution and interphase formation, the exact role of cation substitution in improving the electrochemical performance of iron fluoride cathodes remains elusive. It should also be noted that, despite starting from a solid solution ternary difluoride where all transition metals should have an oxidation state of +2,  $\text{Fe}^{3+}$  have often been detected after the first charge [19], suggesting the structural irreversibility of these cathodes.

One effective approach to addressing the dissolution issue is replacing liquid electrolytes with solid electrolytes to make solid-state batteries [58–65]. The utilization of solid electrolytes can also help mitigate the particle displacement as well as form a less dynamic interphase (no need to reform part of the interphase upon pulverization/cracking), improving the cycling stability of iron fluoride cathodes [66]. Moreover, integrating iron fluoride cathodes with solid electrolytes may provide additional kinetic benefits due to the absence of concentration polarization in the liquid electrolytes and the larger content of  $\text{Li}$  ion per volume of electrolyte [20]. The utilization of polymer-based solid electrolyte helps improve the cycling stability of  $\text{FeF}_2$  cathodes at elevated temperatures ( $50^\circ\text{C}$ ) due to reduced electrolyte decomposition and improved structural stability of the cathode [16]. Recently, Peng et al. reported a high-capacity, long-life  $\text{FeF}_3$  solid state battery based on sulfide-based  $\text{Li}_6\text{PS}_5\text{Cl}$  solid electrolyte [66, 67]. Nevertheless, challenges remain for room temperature operation of polymer-based solid state batteries because of the low ionic conductivity of polymer electrolyte. While a large capacity was achieved for  $\text{FeF}_3$  cathode in sulfide-based solid-state batteries, most of the capacity is delivered at a much lower voltage than the theoretical electrode potential of  $\text{FeF}_3$  [68], suggesting possible side reaction between  $\text{FeF}_3$  with the sulfide electrolytes. Recently, Shao et al. reported the utilization of halide-based  $\text{Li}_3\text{YCl}_6$  solid electrolyte can enable a complete conversion and reconversion of  $\text{FeF}_2$  cathode at its theoretical potential due to the excellent (electro)chemical stability between  $\text{Li}_3\text{YCl}_6$  and  $\text{FeF}_2$  cathode [69]. Solid state  $\text{FeF}_2$  cathode based on  $\text{Li}_3\text{YCl}_6$  solid electrolyte also delivered excellent cycling stability with a low voltage hysteresis, suggesting a promising approach to address the performance limitation of iron fluoride cathodes.

In this work, we aim to understand the role of  $\text{CuF}_2$  and  $\text{NiF}_2$  incorporation in the electrochemical performance of  $\text{FeF}_3$  cathodes with halide-based  $\text{Li}_3\text{YCl}_6$  solid electrolyte. The fundamental question we would like to answer is whether we can achieve the kinetic benefits of cation incorporation in  $\text{FeF}_3$ , which has a higher energy density than  $\text{FeF}_2$ , while suppressing transition metal dissolution and interphase growth by solid-state concept to simultaneously lower voltage hysteresis and improve cycle life. Combining electrochemical analysis and material characterization, we report that the incorporation of  $\text{CuF}_2$  and  $\text{NiF}_2$  in  $\text{FeF}_3$  cathode does not have an apparent effect in improving the electrode kinetics in  $\text{Li}_3\text{YCl}_6$ -based solid state batteries. However, apparent improvement in cycling stability of the  $\text{FeF}_3$  can be achieved probably due to the suppression of transition metal



**FIGURE 1** | XRD patterns of CuF<sub>2</sub>-FeF<sub>3</sub> (a) and NiF<sub>2</sub>-FeF<sub>3</sub> (b). HRTEM image, SAED, and elemental mapping of FeF<sub>3</sub> (c to e), 25CuF<sub>2</sub>-75FeF<sub>3</sub> (f-h), and 10NiF<sub>2</sub>-90FeF<sub>3</sub> (i to k). (l) Fe K-edge XANES spectra of FeF<sub>3</sub>, 25CuF<sub>2</sub>-75FeF<sub>3</sub>, and 10NiF<sub>2</sub>-90FeF<sub>3</sub>. (m) Cu K-edge XANES spectra of 25CuF<sub>2</sub>-75FeF<sub>3</sub>. (n) Ni K-edge XANES spectra of 10NiF<sub>2</sub>-90FeF<sub>3</sub>.

dissolution and improvements in the mechanical stability of the cathodes.

## 2 | Results and Discussion

### 2.1 | Characterizations of FeF<sub>3</sub>, CuF<sub>2</sub>-FeF<sub>3</sub>, and NiF<sub>2</sub>-FeF<sub>3</sub>

The incorporation of CuF<sub>2</sub> and NiF<sub>2</sub> in FeF<sub>3</sub> is achieved by high-energy ball-milling of CuF<sub>2</sub> and NiF<sub>2</sub> with FeF<sub>3</sub> with various molar contents of CuF<sub>2</sub>/NiF<sub>2</sub> from 0% to 100%. The same method was also used to prepare ternary transitional metal fluoride solid solutions [19]. Cu and Ni were chosen as the incorporated cations because the high electrode potential (3.55 V for CuF<sub>2</sub> and 2.96 V for NiF<sub>2</sub>) and theoretical capacity (528 mAh/g for CuF<sub>2</sub> and 554 mAh/g for NiF<sub>2</sub>) [12, 26] to ensure that the potential improvements in kinetics and cycling performance do not largely compromise the energy density. Figure 1a,b shows the XRD patterns of CuF<sub>2</sub> and NiF<sub>2</sub> incorporated FeF<sub>3</sub>. Significant

peak broadening can be observed for all samples containing FeF<sub>3</sub>, suggesting a reduction in particle sizes during high-energy ball-milling (Figure S1). Bragg reflections of FeF<sub>3</sub> (ReO<sub>3</sub>-type structure, space group  $R\bar{3}c$ ) and CuF<sub>2</sub> (monoclinic, space group  $P2_1/n$ )/NiF<sub>2</sub> (tetragonal, space group  $P4_2/mmm$ ) can be observed for all mixed fluorides with no impurity phases. No apparent peak shift can be observed for each phase. The results suggest the CuF<sub>2</sub>-FeF<sub>3</sub> and NiF<sub>2</sub>-FeF<sub>3</sub> are most likely nanocomposites of the difluoride and FeF<sub>3</sub>, instead of substitution. It should be noted that a rutile-like Cu-Fe-F compound with the oxidation state of Cu and Fe being +2 and +3, respectively, was reported as the product after charging Cu<sub>0.5</sub>Fe<sub>0.5</sub>F<sub>2</sub> solid solution to 4.5 V [19]. Such a rutile compound is not observed in the XRD results.

HRTEM was used to probe the structure of FeF<sub>3</sub>, 25CuF<sub>2</sub>-5FeF<sub>3</sub>, and 10NiF<sub>2</sub>-90FeF<sub>3</sub> (Figure 1c-k). All three mixed fluorides show agglomeration of highly crystalline nanoparticles with a size of 5–10 nm (Figure 1c,f,i). Lattice fringes with interplanar spacing corresponding to FeF<sub>3</sub>, CuF<sub>2</sub>, and NiF<sub>2</sub> can be observed in the mixed fluorides. The presence of CuF<sub>2</sub> and NiF<sub>2</sub> in the

mixed fluorides is also confirmed from the selected area electron diffraction (SAED) (Figure 1d,g,j), consistent with the XRD results (Figure 1a,b) that the  $25\text{CuF}_2-75\text{FeF}_3$  and  $10\text{NiF}_2-90\text{FeF}_3$  are composites in nature. The composite feature of the mixed fluorides was also supported by the EDS results (Figure 1e,h,k), which show nonuniform distribution of Fe and Cu/Ni in  $25\text{CuF}_2-75\text{FeF}_3$  and  $10\text{NiF}_2-90\text{FeF}_3$ . It should be noted that the particle size of  $\text{CuF}_2$  was observed to be much smaller than  $\text{FeF}_3$  and  $\text{NiF}_2$ , and this help explain the weak diffractions from both SAED (Figure 1h) and XRD (Figure 1a), although the molar content of  $\text{CuF}_2$  in  $25\text{CuF}_2-75\text{FeF}_3$  is higher than that of  $\text{NiF}_2$  in  $10\text{NiF}_2-90\text{FeF}_3$ .

To understand the effect of  $\text{CuF}_2/\text{NiF}_2$  incorporation on the electronic structure of transition metals, we also measured the synchrotron X-ray absorption near edge structure (XANES) of Fe K-edge (Figure 1l), Cu K-edge (Figure 1m), and Ni K-edge (Figure 1n) in  $\text{FeF}_3$ ,  $25\text{CuF}_2-75\text{FeF}_3$ , and  $10\text{NiF}_2-90\text{FeF}_3$ . Reference XANES spectra of commercial metals (Fe, Cu, and Ni) and metal fluorides ( $\text{FeF}_2$ ,  $\text{FeF}_3$ ,  $\text{CuF}_2$ , and  $\text{NiF}_2$ ) were also measured as reference. Although slight shift of the absorption edge to lower energies can be observed, the line shape of Fe K-edge XANES spectra in  $\text{FeF}_3$ ,  $25\text{CuF}_2-75\text{FeF}_3$ , and  $10\text{NiF}_2-90\text{FeF}_3$  are quite similar to that of the micron-sized  $\text{FeF}_3$  (Figure 1l). The underlying reason for the slight shift of the absorption edge of Fe for  $25\text{CuF}_2-75\text{FeF}_3$  and  $10\text{NiF}_2-90\text{FeF}_3$  to a lower energy is currently unknown but might be due to slight doping of Fe into  $\text{NiF}_2/\text{CuF}_2$ , which can lead to slight reduction of Fe. The XANES spectra of Cu K-edge of  $25\text{CuF}_2-75\text{FeF}_3$  (Figure 1m) and Ni K-edge of  $10\text{NiF}_2-90\text{FeF}_3$  (Figure 1n) are also similar to that of  $\text{CuF}_2$  and  $\text{NiF}_2$  reference spectra, respectively, further confirming the mixed fluoride are largely composite in nature.

## 2.2 | Effect of $\text{CuF}_2/\text{NiF}_2$ Incorporation on the Electrochemical Performance of $\text{FeF}_3$

To measure the electrochemical performance,  $\text{FeF}_3$ ,  $\text{CuF}_2-\text{FeF}_3$ , and  $\text{NiF}_2-\text{FeF}_3$  were first mixed with vapor grown carbon fiber (VGCF) and then  $\text{Li}_3\text{YCl}_6$  solid electrolytes, both by a ball-milling process, to make composite cathodes. The electrochemical performance of  $\text{FeF}_3$ ,  $\text{CuF}_2-\text{FeF}_3$  and  $\text{NiF}_2-\text{FeF}_3$  composite cathodes were measured by galvanostatic cycling at various current densities in a solid-state cell with  $\text{Li}_3\text{YCl}_6$  solid electrolyte and Li-In anode at  $60^\circ\text{C}$ . The active material loading for each cell is fixed at around  $2.6\text{ mg/cm}^2$ . Figure 2a,b compares the charge/discharge curves for the second cycle of  $\text{CuF}_2-\text{FeF}_3$  and  $\text{NiF}_2-\text{FeF}_3$  cathodes with those of  $\text{FeF}_3$  cathode. Two typical voltage plateaus,  $\sim 3.4-3.6\text{ V}$  and  $\sim 1.7\text{ V}$  during discharge and  $\sim 2.6$  and  $\sim 3.7\text{ V}$  during charge can be observed in the charge/discharge profiles of  $\text{FeF}_3$ , as also shown in the cyclic voltammetry results (Figure S2). The specific capacity for is  $693\text{ mAh/g}$  for discharge and  $612\text{ mAh/g}$  for discharge. The reversible capacity is close to the theoretical capacity ( $712\text{ mAh/g}$ ), although part of the capacity may be from the reversible decomposition of  $\text{Li}_3\text{YCl}_6$  solid electrolyte as a higher reversible capacity can be observed for the first cycle (Figure S3). The incorporation of  $\text{CuF}_2$  leads to decreases of overall capacity (Figure 2c). On the other hand, the incorporation of  $\text{NiF}_2$  leads to decreases in the specific capacities in the high-voltage-plateau region, due to the reduced contribution from  $\text{FeF}_3$  intercalation, and increase in the specific capacities of in the low-voltage-

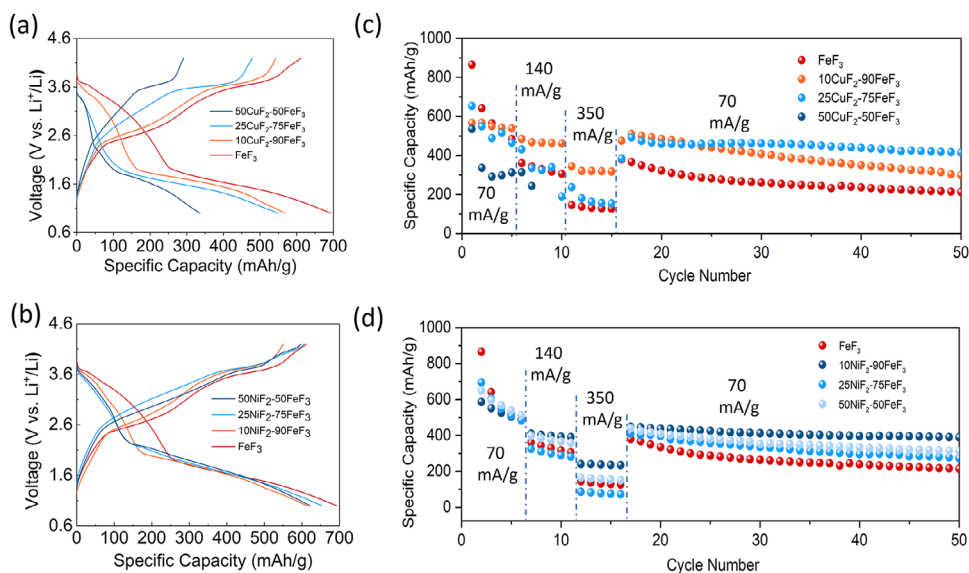
plateau region due to additional redox from  $\text{NiF}_2$  conversion (Figure 2d). A much larger capacity decrease can be observed for  $\text{CuF}_2-\text{FeF}_3$  cathodes than  $\text{NiF}_2-\text{FeF}_3$  at the same molar contents. It should be noted that increasing the  $\text{NiF}_2$  content does not lead to a proportional decrease in discharge capacity (Figure 2d), despite its lower theoretical capacity compared to  $\text{FeF}_3$ , possibly due to the role of  $\text{NiF}_2$  conversion in promoting the utilization of  $\text{FeF}_3$  during discharge, for example, by generating electrically conductive Ni prior to the conversion of  $\text{FeF}_2$ .

Nevertheless, we do not observe reduction in the voltage hysteresis after  $\text{CuF}_2/\text{NiF}_2$  incorporation (Figure 2a,b). Both  $\text{CuF}_2-\text{FeF}_3$  and  $\text{NiF}_2-\text{FeF}_3$  showed a higher voltage hysteresis than  $\text{FeF}_3$  (Figure S4). The results suggest that the kinetic benefits of mixed difluoride solid solutions in liquid electrolyte cannot be transferred to the mixed trifluoride nanocomposites. Nevertheless, the incorporation of  $\text{CuF}_2$  and  $\text{NiF}_2$  are beneficial to improve the cycling performance of  $\text{FeF}_3$  cathode in  $\text{Li}_3\text{YCl}_6$ -based solid-state batteries (Figure 2c,d). The charge/discharge curves for the cycling performance tests at different current densities are shown in Figure S5. All  $\text{NiF}_2$ -containing cathodes showed improved cycling stability than  $\text{FeF}_3$  cathode (Figure 2d). For  $\text{CuF}_2$ -containing cathodes, the cycling stability first increases and then decreases with  $\text{CuF}_2$  content with  $\text{FeF}_3$  cathode, with 25 mol%  $\text{CuF}_2$  exhibiting the best cycling stability for the first 50 cycles (Figure 2c). Given the excellent performance of  $10\text{NiF}_2-90\text{FeF}_3$  and  $25\text{CuF}_2-75\text{FeF}_3$  cathodes, we then focused on these two cathodes to understand the effects of  $\text{CuF}_2/\text{NiF}_2$  incorporation on the kinetics and cycling stability of  $\text{FeF}_3$ .

## 2.3 | Effect of $\text{CuF}_2/\text{NiF}_2$ Incorporation on the Reaction Mechanism of $\text{FeF}_3$ Cathodes

The electronic structure of the  $\text{FeF}_3$ ,  $25\text{CuF}_2-75\text{FeF}_3$ , and  $10\text{NiF}_2-90\text{FeF}_3$  cathode composites were probed by XANES spectra of Fe, Cu, and Ni K-edge. We first compared the XANES spectra of the composite cathodes with those of the  $\text{FeF}_3$ ,  $25\text{CuF}_2-75\text{FeF}_3$ , and  $10\text{NiF}_2-90\text{FeF}_3$  active materials (Figure 1l-n) to investigate the chemical stability between the active material and  $\text{Li}_3\text{YCl}_6$  solid electrolyte during fabrication of the cathode composite through ball milling. For Fe-K edge, the absorption edge of XANES spectra of all pristine cathode composites (Figure 3a,b,d) shifted to a lower energy that corresponds to  $\text{Fe}^{2+}$ , suggesting the reduction of Fe from  $\text{Fe}^{3+}$  to  $\text{Fe}^{2+}$ . The reduction of Cu, to form  $\text{Cu}^+$  species, can also be observed based on the shift of the absorption edge of Cu K edge (Figure 3c), while the oxidation state of Ni remains +2 in the  $10\text{NiF}_2-90\text{FeF}_3$  (Figure 3e). The results suggest the instability of the  $\text{FeF}_3$ -based cathodes with  $\text{Li}_3\text{YCl}_6$  solid electrolyte during cathode composite fabrication.

To understand the effect of  $\text{CuF}_2/\text{NiF}_2$  incorporation in the reaction mechanism of  $\text{FeF}_3$ , we measured the XANES spectra of  $\text{FeF}_3$ ,  $10\text{NiF}_2-90\text{FeF}_3$ , and  $25\text{CuF}_2-75\text{FeF}_3$  composite cathodes at the fully discharged and fully charged states (Figure 3a-e). For  $\text{FeF}_3$  cathode, after discharge to  $1.0\text{ V vs. Li/Li}^+$ , the Fe K-edge XANES spectrum exhibits a pronounced shift of the absorption edge toward lower energy, accompanied by a substantial change in line shape (Figure 3a). The edge position and post-edge features approach those of metallic Fe, indicating a reduction of  $\text{Fe}^{2+}$  to  $\text{Fe}^0$  during the conversion reaction. The oxidation of Fe from



**FIGURE 2** | Charge/discharge curves of  $\text{CuF}_2\text{-FeF}_3$  (a) and  $\text{NiF}_2\text{-FeF}_3$  (b) in  $\text{Li}_3\text{YCl}_6$ -based solid-state batteries at 70 mA/g. Cycling performance of  $\text{CuF}_2\text{-FeF}_3$  (c) and  $\text{NiF}_2\text{-FeF}_3$  (d) in  $\text{Li}_3\text{YCl}_6$ -based solid-state batteries at various current densities. Li-In was used as the anode, and the electrochemical performances were measured at 60°C.

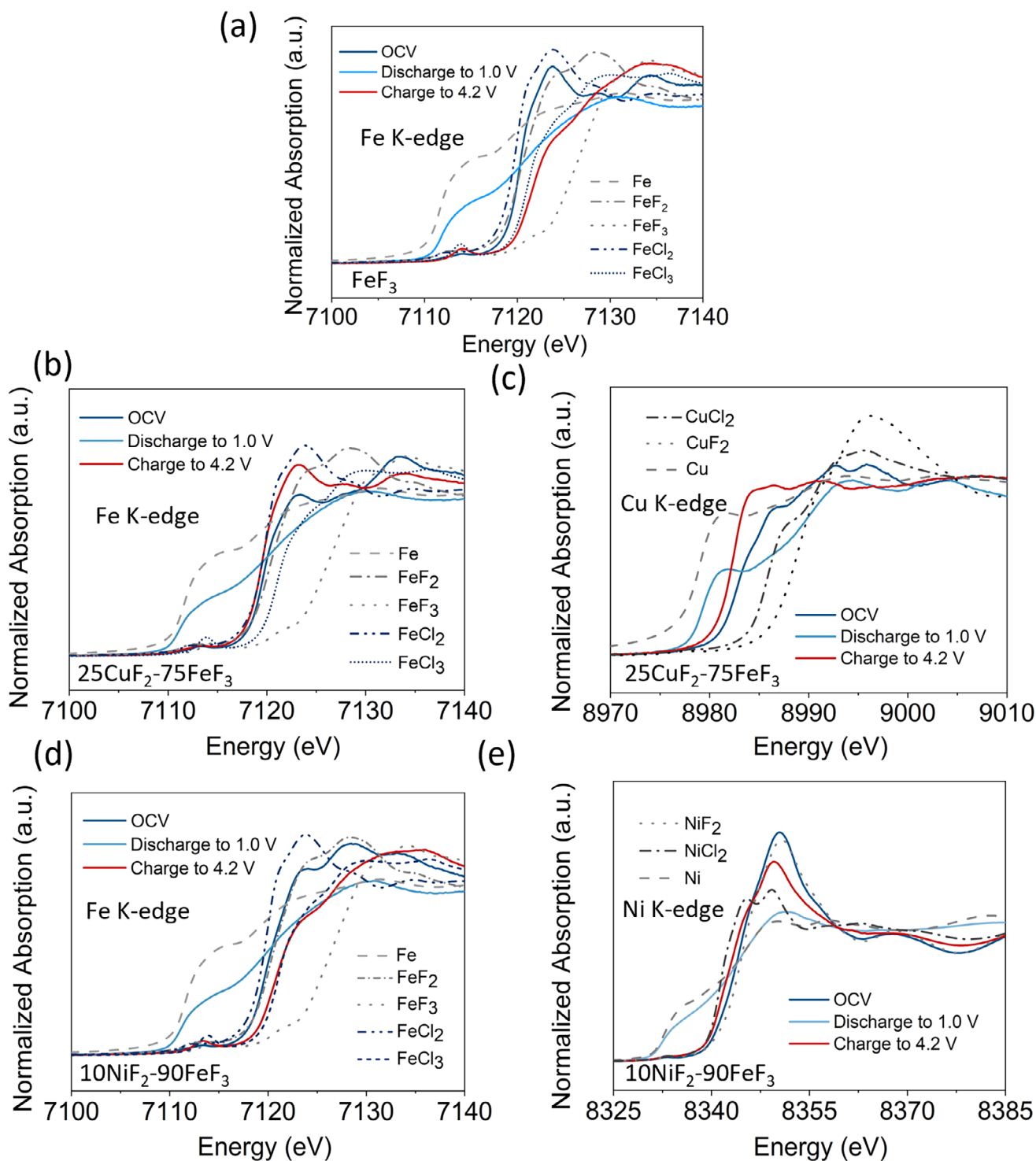
$\text{Fe}^0$  to  $\text{Fe}^{3+}$  can be observed after charging to 4.2 V, based on the shift of the absorption edge to a higher energy (Figure 3a). However, comparing the line shape of the spectrum with the XANES spectra of  $\text{FeCl}_3$  and  $\text{FeF}_3$  reference samples, Fe in the fully charged electrode mainly exists as  $\text{FeCl}_3$ , rather than  $\text{FeF}_3$ , indicating that the electrochemical reaction between  $\text{FeF}_3$  and  $\text{Li}_3\text{YCl}_6$  also occurred during the charge/discharge processes. The results are consistent with a prior study that reports a large content of  $\text{FeCl}_3$  after charging  $\text{FeF}_2\text{-Li}_3\text{YCl}_6$  cathode to 4.0 V vs.  $\text{Li}/\text{Li}^+$  [69]. Complete reduction from  $\text{Fe}^{2+}$  to  $\text{Fe}^0$  can also be observed in the  $25\text{CuF}_2\text{-75FeF}_3$  and  $10\text{NiF}_2\text{-90FeF}_3$  composite cathodes. However, after charging, Fe in  $25\text{CuF}_2\text{-75FeF}_3$  will be oxidized to  $\text{Fe}^{2+}$  in the form of  $\text{FeCl}_2$  (Figure 3b) while for  $10\text{NiF}_2\text{-90FeF}_3$  the Fe will be oxidized to  $\text{FeCl}_3$  with an oxidation state of +3 (Figure 3d). The formation of  $\text{FeCl}_3$  is believed to be reversible due to the very similar charge profile of the second cycle when compared with that of the first cycle. The evolution of XANES of Cu K-edge (Figure 3c) indicates the reduction of  $\text{Cu}^+$  to  $\text{Cu}^0$  after discharge and the oxidation of  $\text{Cu}^0$  to  $\text{Cu}^+$  after charge. Interestingly, the absorption edge of XANES of Cu K-edge for the fully charged  $25\text{CuF}_2\text{-75FeF}_3$  appears at a lower energy than that of the pristine sample (Figure 3c), which is likely due to the change in the local environment of  $\text{Cu}^+$  from  $\text{CuF}$ -like species in the pristine electrode to  $\text{CuCl}$ -like species in the fully charged electrode. The XANES spectra of Ni K-edge (Figure 3e) show a reduction from  $\text{NiF}_2$  to Ni during discharge and oxidation back to  $\text{NiF}_2$  during charge, indicative of a complete conversion and reconversion of  $\text{NiF}_2$  during charge/discharge process.

The above XAS analysis highlights the complexity of the chemical and electrochemical stability between the  $\text{FeF}_3$ -based cathodes and  $\text{Li}_3\text{YCl}_6$  solid electrolytes. The results show clear involvement of Cu and Ni redox processes during charge and discharge process and indicate the significant role of electrochemical stability of  $\text{Li}_3\text{YCl}_6$  in the reaction pathway of the  $\text{FeF}_3$ -based cathodes. Complete oxidation from  $\text{Fe}^0$  to  $\text{Fe}^{3+}$  can be achieved in  $\text{FeF}_3$  and  $10\text{NiF}_2\text{-90FeF}_3$ , while in  $25\text{CuF}_2\text{-75FeF}_3$   $\text{Fe}^0$  can only be oxidized

to  $\text{Fe}^{2+}$  at the fully charged states. The results also help explain the slightly lower discharge plateau of  $25\text{CuF}_2\text{-75FeF}_3$  than that of  $\text{FeF}_3$  and  $10\text{NiF}_2\text{-90FeF}_3$  for the second cycle (Figure 2; Figure S2). For  $\text{FeF}_3$  and  $10\text{NiF}_2\text{-90FeF}_3$ , the high voltage plateau is mainly attributed to the reduction of  $\text{Fe}^{3+}$  to  $\text{Fe}^{2+}$  while in  $\text{CuF}_2\text{-FeF}_3$  it is related to the reduction of  $\text{Cu}^+$ . The low-voltage plateau, however, for all three electrodes, can be attributed to the reduction of  $\text{Fe}^{2+}$  to  $\text{Fe}^0$ .

#### 2.4 | Effect of $\text{CuF}_2/\text{NiF}_2$ Incorporation on Electrode Kinetics of $\text{FeF}_3$ Cathodes

To understand the effect of cation incorporation on electrode kinetics, we also performed galvanostatic intermittent titration technique (GITT) of the cathodes during the second cycle. The quasi-equilibrium voltage profiles, shown in the shaded region, show low voltage hysteresis for all three cathodes (Figure 4a–c), suggesting the voltage hysteresis for these cathodes in  $\text{Li}_3\text{YCl}_6$ -based solid-state batteries is kinetic in nature. The kinetics of the electrode can be reflected by the overpotential, which is the difference of the potential before and after rest, during charge and discharge (Figure S6). Figure 4d compares the evolution of overpotential during charge and discharge of the second cycle. All three cathodes show similar trend with the depth of discharge (DOD). The overpotentials first increase when the electrodes are discharged to 30% DOD, decrease to 45%, increase to 80%, and then slightly decrease until 100% DOD. A similar trend was also observed in previous GITT study of  $\text{FeF}_3$  electrode in liquid electrolyte [11, 14]. The largest overpotential is observed at around the transition point between high-voltage-plateau and low-voltage plateau, and this is probably attributed to the kinetic barrier for nucleation Fe and LiF. During charge, the overpotential first increase to the maximum, decrease at around 80% SOC with a slight increase until the end of charge. Comparing the magnitude of the overpotential,  $25\text{CuF}_2\text{-75FeF}_3$  shows the largest overpotential across the states of charge, while  $10\text{NiF}_2\text{-90FeF}_3$

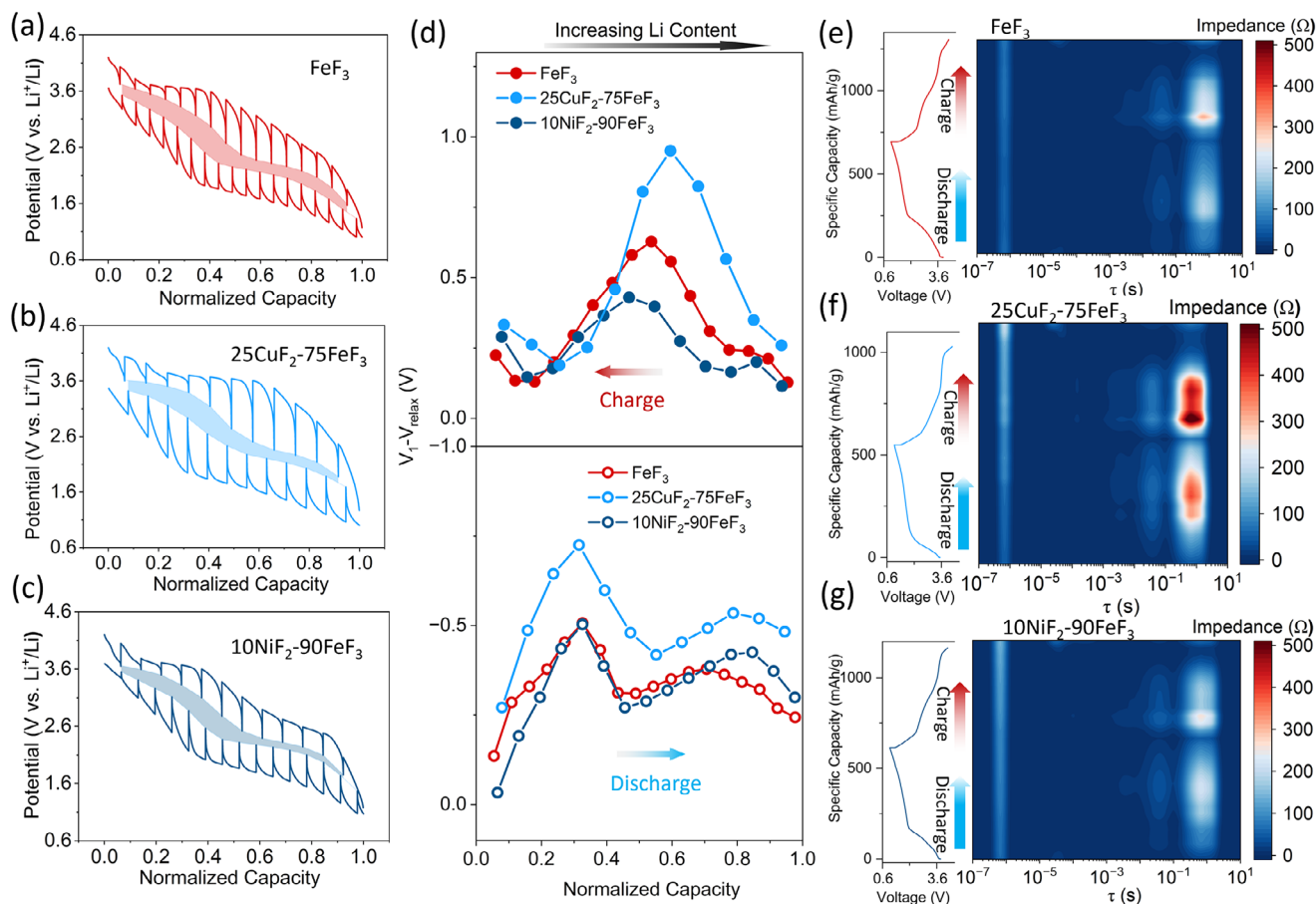


**FIGURE 3** | Near-edge XAS spectra (XANES) for the Fe K-edge, Cu K-edge and Ni K-edge of  $\text{FeF}_3$ ,  $25\text{CuF}_2-75\text{FeF}_3$ , and  $10\text{NiF}_2-90\text{FeF}_3$  electrodes after discharge and charge.

exhibit a slight lower but comparable overpotential with that of  $\text{FeF}_3$ .

To further validate the kinetic analysis through GITT, we also calculated the distribution of relaxation times (DRT) based on the electrochemical impedance spectra (Figures S7–S9) for  $\text{FeF}_3$ ,  $25\text{CuF}_2-75\text{FeF}_3$ , and  $10\text{NiF}_2-90\text{FeF}_3$  during discharge and charge of the second cycle. Figure 4e,f shows the 2D DRT map of the cath-

odes. Based on the DRT result of a Li-In|LYC|Li-In reference cell (Figure S10), the cathode/electrolyte interfacial resistance can be represented by the peak at a characteristic time of 1 s. The results from DRT are consistent with the GITT analysis (Figure 4d). Similar asymmetry of the kinetics for charge and discharge can be observed based on the evolution of the impedance corresponding to a characteristic time of 1 s in Figure 4e,f. Incorporating  $\text{CuF}_2$  in  $\text{FeF}_3$  led to large increases in the cathode/electrolyte interfacial



**FIGURE 4** | GITT analysis of  $\text{FeF}_3$  (a),  $25\text{CuF}_2-75\text{FeF}_3$  (b),  $10\text{NiF}_2-90\text{FeF}_3$  (c) during discharge and charge for the second cycle. (d) Evolution of the overpotential, determined from the GITT measurement, during charge and discharge. 2D DRT surface of  $\text{FeF}_3$  (e),  $25\text{CuF}_2-75\text{FeF}_3$  (f), and  $10\text{NiF}_2-90\text{FeF}_3$  (g) during charge and discharge for the second cycle.

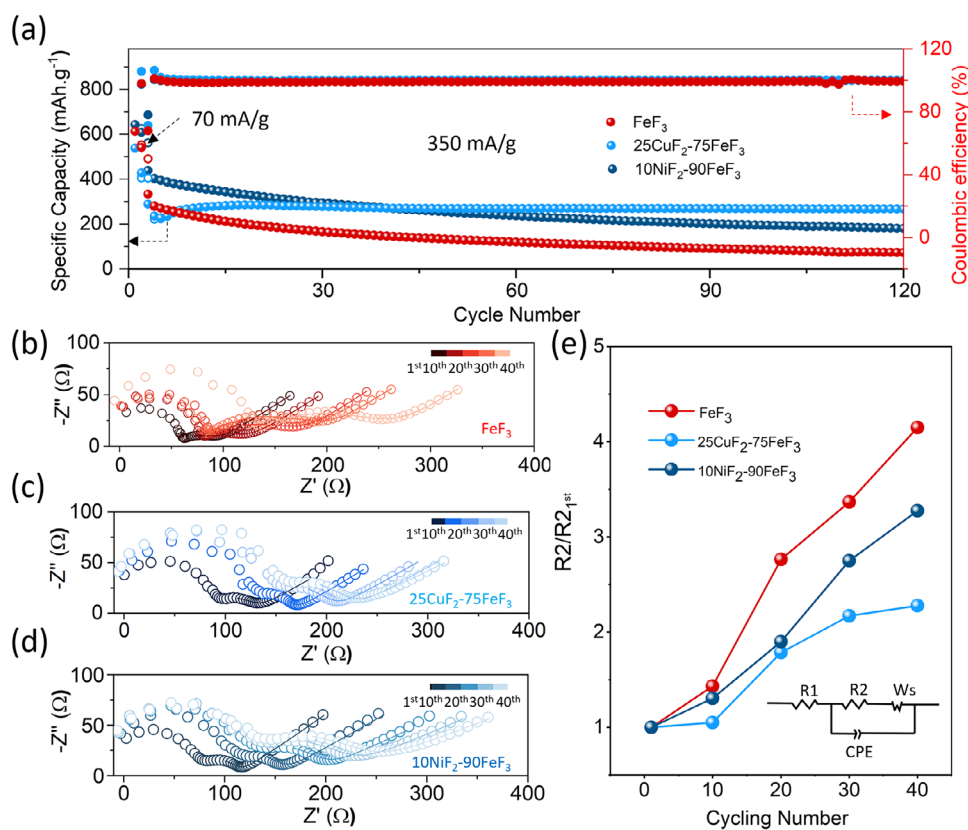
resistances, although a slight lower impedance can be observed for the  $10\text{NiF}_2-90\text{FeF}_3$  cathode. The results further validate that the incorporation of Cu and Ni cannot effectively improve the kinetics of  $\text{FeF}_3$  cathodes.

Correlating with the XANES results, we believe the more sluggish kinetics for  $25\text{CuF}_2-75\text{FeF}_3$  is primarily due to the difference in the reaction mechanisms. While the low-voltage plateau for all three cathodes corresponds to oxidation of Fe to  $\text{Fe}^{2+}$ , the reaction mechanisms for the high voltage plateau are different. For  $\text{FeF}_3$  and  $10\text{NiF}_2-90\text{FeF}_3$ , it is attributed of oxidation of  $\text{Fe}^{2+}$  to  $\text{Fe}^{3+}$  and Ni to  $\text{Ni}^{2+}$  but is corresponding to oxidation of Cu to  $\text{Cu}^+$  for  $25\text{CuF}_2-75\text{FeF}_3$ . We suspect the origin of the sluggish kinetics of  $25\text{CuF}_2-75\text{FeF}_3$  is attributed to the large particle of Cu, given that Cu has a more apparent coarsening effect than Ni and Fe due to its higher homologous temperature at the testing temperature ( $60^\circ\text{C}$ ). Despite that, no apparent feature of  $\text{Cu}^0$  can be observed in the Cu K-edge XANES of the fully charged  $\text{CuF}_2-\text{FeF}_3$  cathode, suggesting that even though the kinetics is sluggish, all  $\text{Cu}^0$  can be oxidized, which is sharply different from the results in liquid electrolytes where residual  $\text{Cu}^0$  can be observed for the charging  $\text{CuF}_2-\text{FeF}_3$  cathode even to 4.5 V vs.  $\text{Li}^+/\text{Li}^+$  [19]. The result implies that the utilization of solid electrolytes may suppress the growth of Cu nanoparticles compared to liquid electrolytes, i.e., although Cu still grows, it does not grow as fast as in liquid electrolyte batteries. Another possible reason for the different electrode

kinetics in solid state and liquid electrolyte batteries might be related to Cu dissolution. While dissolution is not desired for improving cycling stability, it can help reaction kinetics, such as in liquid-electrolyte lithium sulfur batteries, especially given that the conversion reaction of  $\text{CuF}_2$  is topotactic transformation in nature involving the transport of both Li and Cu [25].

## 2.5 | Effect of $\text{CuF}_2/\text{NiF}_2$ Incorporation on Cycling Stability of $\text{FeF}_3$ Cathodes

Although no apparent improvement in kinetics can be observed, we did observe a large improvement in the cycling stability after  $\text{CuF}_2/\text{NiF}_2$  incorporation (Figure 2c,d). The improvement in the cycling performance was further validated by long-cycling tests of  $\text{FeF}_3$ ,  $25\text{CuF}_2-75\text{FeF}_3$ , and  $10\text{NiF}_2-90\text{FeF}_3$  at 0.5 C (Figure 5a).  $25\text{CuF}_2-75\text{FeF}_3$  demonstrates the best cycling stability with minimal capacity decay for more than 100 cycles. It has been reported that the incorporation of  $\text{NiF}_2$  into  $\text{FeF}_2$  led to quick capacity decay for the first 25 cycles in liquid electrolyte batteries due to the significant growth of cathode electrolyte interphase [21, 23], and Cu-containing  $\text{FeF}_2$  can be cycled for a few times in liquid electrolyte due to Cu dissolution [19, 55]. While a fast capacity decay can also be observed in solid-state cells for the first few cycles (Figure 5a) arising from microstructural and interphase stabilization due to the (electro)chemical instability between the



**FIGURE 5** | (a) Cycling performance and coulombic efficiency of FeF<sub>3</sub>, 25CuF<sub>2</sub>-75FeF<sub>3</sub>, and 10NiF<sub>2</sub>-90FeF<sub>3</sub>. (b–d) Nyquist plots collected from the first to the 100th cycle at intervals of 10 cycles, showing progressive impedance growth for FeF<sub>3</sub> (b), 25CuF<sub>2</sub>-75FeF<sub>3</sub> (c), and 10NiF<sub>2</sub>-90FeF<sub>3</sub> (d). (e) Cathode/electrolyte impedances after cycling 10, 20, 30, and 40 times.

solid electrolyte and the electrodes, the capacity can quickly stabilize for the first few cycles. The cycling performances of solid state 25CuF<sub>2</sub>-75FeF<sub>3</sub> and 10NiF<sub>2</sub>-90FeF<sub>3</sub> cathode represent a significant improvement, suggesting the advantages of using solid electrolyte to improve the cycling performance by forming a less dynamic interphase and eliminating transition metal dissolution. It should be noted that the less dynamic feature of the interphase formation in solid-state batteries mainly arise from the elimination of continuous reformation of the interphase upon cracking or pulverization due to non-infiltrative features of solid electrolytes compared to liquids. However, it does not suggest that the solid electrolyte will be more (electro)chemically stable with the electrode than liquid electrolytes. The (electro)chemical instability between Li<sub>3</sub>YCl<sub>6</sub> and FeF<sub>3</sub>-based solid electrolyte also led to irreversible formation of LiF that remains in the cathode composite, and the existence of LiF may play a role in stabilizing the interface due to its excellent stability. The average coulombic efficiency of FeF<sub>3</sub>, 25CuF<sub>2</sub>-75FeF<sub>3</sub>, and 10NiF<sub>2</sub>-90FeF<sub>3</sub> during long-term cycling are 99.1%, 100.0%, and 99.6%, respectively. The results suggest that the incorporation of CuF<sub>2</sub> and NiF<sub>2</sub> helps to improve the reversibility during charge and discharge, which in turn leads to an enhanced cycling stability of the cathode. The high coulombic efficiencies for all three cathodes also suggest the stability of the interphase after it was formed for the first few cycles.

The excellent cycling performance after CuF<sub>2</sub>/NiF<sub>2</sub> incorporation is also supported by the impedance evolution after different cycles (Figure 5b–d). The second semicircle corresponds to the interfa-

cial resistance between cathode and solid electrolyte. While the initial cathode/electrolyte interfacial resistance of FeF<sub>3</sub> (12.9 Ω) is lower than that of 25CuF<sub>2</sub>-75FeF<sub>3</sub> (55.7 Ω) and 10NiF<sub>2</sub>-90FeF<sub>3</sub> (39.6 Ω) due to its better kinetics for the first few cycles, as also demonstrated in the GITT and DRT analysis (Figures 4 and 5), it increases faster during long-term cycling. The increase rate of the impedance is consistent with the cycling performance, with the 25CuF<sub>2</sub>-75FeF<sub>3</sub> exhibiting the lowest impedance increase for the first 40 cycles.

The exact mechanism for the enhanced cycling stability after CuF<sub>2</sub>/NiF<sub>2</sub> incorporation is currently unknown but may be related to the mitigated electro-chemo-mechanical degradation, which has been considered as one key source for the cycling instability of solid-state electrodes [70–72]. The incorporation of CuF<sub>2</sub> and NiF<sub>2</sub> can lead to multiple redox centers occurring at different voltage, and more importantly at different locations of the electrodes, depending on the distribution of transition metals in the electrode. Instead of lithiation or delimitation between Fe<sup>0</sup> and Fe<sup>3+</sup> at a single site, the capacity of the electrode can be achieved by redox behavior at different sites and potentials. Such cooperative redox behavior will help reduce the strain/stress generated in the electrode composite, thus mitigating the contact loss due to the electro-chemo-mechanical degradation during long term cycling. Similar concept has been demonstrated in mixed transition metal oxide for conversion anodes [73]. More careful characterizations to understand the pressure evolution during long term charge/discharge cycles and to correlate it with the microstructure evolution especially at the cathode/electrolyte

interfaces would be very helpful to validate this mechanism. Additional mechanisms that may help improve the cycling stability include the formation of more passivating interphase after incorporating  $\text{CuF}_2/\text{NiF}_2$ , which is supported by the improved coulombic efficiency during long-term cycling.

### 3 | Conclusions

We investigated the effect of  $\text{CuF}_2$  and  $\text{NiF}_2$  incorporation in electrochemical performance of  $\text{FeF}_3$  cathodes in  $\text{Li}_3\text{YCl}_6$ -based solid-state batteries. The difference in the structure of  $\text{CuF}_2/\text{NiF}_2$  and  $\text{FeF}_3$  led to the formation of a nanocomposite of these fluorides. Different from the previous report on the enhanced electrode kinetics of ternary metal fluorides in liquid electrolyte batteries, no apparent decrease in voltage hysteresis can be observed after incorporation of  $\text{CuF}_2$  or  $\text{NiF}_2$  in  $\text{FeF}_3$  in solid-state batteries. The XANES results confirmed the involvement of Cu ( $\text{Cu}^0/\text{Cu}^+$ ) and Ni ( $\text{Ni}^0/\text{Ni}^{2+}$ ) redox behaviors in the mixed fluorides. While the oxidation of Fe from  $\text{Fe}^0$  to  $\text{Fe}^{3+}$  can be observed for  $\text{FeF}_3$  and  $10\text{NiF}_2\text{-}90\text{FeF}_3$  after charging to 4.2 V vs.  $\text{Li}/\text{Li}^+$ , only  $\text{Fe}^{2+}$  can be observed in fully charged  $\text{CuF}_2\text{-FeF}_3$ . The results suggest the complex reaction mechanisms of solid-state  $\text{FeF}_3$ ,  $25\text{CuF}_2\text{-}75\text{FeF}_3$ , and  $10\text{NiF}_2\text{-}90\text{FeF}_3$  electrodes, involving significant (electro)chemical reactions with  $\text{Li}_3\text{YCl}_6$  solid electrolytes. The effect of  $\text{CuF}_2/\text{NiF}_2$  incorporation on electrode kinetics was also studied by GITT and DRT analysis. While  $10\text{NiF}_2\text{-}90\text{FeF}_3$  demonstrated comparable kinetic performance with  $\text{FeF}_3$ , the overpotential and impedance of  $25\text{CuF}_2\text{-}75\text{FeF}_3$  are much higher, probably due to the different reaction mechanisms of these mixed fluorides. Nevertheless, significant improvement in the cycling performance can be observed after incorporating  $\text{CuF}_2$  and  $\text{NiF}_2$  in  $\text{FeF}_3$ , likely due to the mitigation of electro-chemo-mechanical degradations from the cooperative redox behavior of additional transition metal in solid-state batteries. The work highlights the unique advantages of using solid state concept to improve the cycling performance of  $\text{FeF}_3$  cathodes and provides novel insights for developing  $\text{FeF}_3$  cathodes for solid-state batteries.

## 4 | Experimental Section

### 4.1 | Materials Synthesis

Commercial  $\text{FeF}_3$  ( $\geq 97\%$ , Sigma-Aldrich),  $\text{NiF}_2$  ( $\geq 99\%$ , Alfa Aesar), and  $\text{CuF}_2$  ( $\geq 99\%$ , Sigma-Aldrich) were used as starting materials without further purification.  $\text{NiF}_2\text{-FeF}_3$  and  $\text{CuF}_2\text{-FeF}_3$  composites were prepared by high-energy ball milling. Specifically, stoichiometric amounts of  $\text{FeF}_3$  and  $\text{NiF}_2$  (or  $\text{CuF}_2$ ) were weighed according to the desired molar ratios (10:90, 25:75, 50:50), sealed in a stainless steel jar with 10 balls under an Ar-filled glovebox, and milled at 300 rpm for 12 h with a ball-to-powder weight ratio of 60:1. The resulting powders were collected and stored in an argon atmosphere to prevent moisture uptake.

### 4.2 | Materials Characterization

Powder X-ray diffraction (XRD, Panalytical Empyrean,  $\text{Cu K}\alpha$  radiation) was used to analyze phase structures. Scanning electron microscopy (SEM, Carl Zeiss Supra 55) coupled with energy-

dispersive X-ray spectroscopy (EDX) was employed to examine morphology and elemental distribution. Transmission electron microscopy (TEM) and high-resolution/atomic-resolution TEM (JEOL F200) were used to investigate microstructure, lattice fringes, and nanoscale elemental distribution. The K-edge XAS spectra of Fe, Cu, and Ni were measured in fluorescence mode at 7-BM beamline (QAS) of National Synchrotron Light Source II (NSLS II), Brookhaven National Laboratory (BNL), using standard references (Fe,  $\text{FeF}_2$ ,  $\text{FeF}_3$ , Ni,  $\text{NiF}_2$ , Cu,  $\text{CuF}_2$ ) for comparison. The data was analyzed using the Athena software.

### 4.3 | Electrochemical Measurements

Composite cathodes were prepared by mixing active material ( $\text{FeF}_3$  or  $\text{NiF}_2/\text{CuF}_2\text{-FeF}_3$  composite), vapor-grown carbon fibers (VGCF), and  $\text{Li}_3\text{YCl}_6$  (LYC) in a weight ratio of 4:2:4. LYC is also prepared by ball milling at 500 rpm for 55 h in  $\text{ZrO}_2$  jars with a ball-to-powder weight ratio of 30:1 as we reported in the previous work [69, 74]. The mixture was prepared by ball milling with active materials and VGCF at 380 rpm for 10 h and then with LYC at 360 rpm for 1.5 h. All-solid-state cells were assembled in an Ar-filled glovebox ( $<0.1$  ppm  $\text{O}_2$  and  $\text{H}_2\text{O}$ ). The LYC (120 mg) was pressed into pellets (diameter 10 mm) under 100 MPa for 3 min. The cathode layer (5 mg) was uniformly spread on one side of the pellet under 300 MPa for 3 min, followed by an In-Li alloy powder anode on the other side (500 mg). The stacked cell was pressed under 350 MPa for 1 min to ensure intimate contact. Galvanostatic charge-discharge cycling was carried out using a LAND battery tester in the voltage range of 1.0–4.2 V (vs.  $\text{Li}^+/\text{Li}$ ). Rate performance was tested at current densities of 70, 140, and 350 mA/g, followed by recovery at 0.1 C (1 C = 712 mAh/g). The GITT test was conducted by applying a constant current of 0.1424 mA/g for 30 min, followed by an open-circuit relaxation for 10 h using an Arbin system. EIS spectra at each relaxation step during the GITT test using a Gamry instrument. At each potential step, the cell was held for 5 h to reach a quasi-steady state before applying an AC perturbation over the frequency range of 10 MHz to 0.01 Hz. CV was measured on a Bio-Logic VMP3 potentiostat at a scan rate of 0.01  $\text{mV s}^{-1}$ .

### Author Contributions

Fudong Han conceived the idea and supervised the project. K.X. prepared the materials, performed the electrochemistry tests, and conducted the XRD, SEM, and EDX analysis. Ru Xiao assisted with the DRT analysis. K.X. and Enyuan Hu performed the XAS tests. K.X. and Fudong Han wrote the manuscript with the input of all the co-authors.

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## Conflicts of Interest

None of the authors have a conflict of interest to disclose.

## Data Availability Statement

The data that support the findings of this study are available from the corresponding author upon reasonable request.

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### Supporting Information

Additional supporting information can be found online in the Supporting Information section.

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